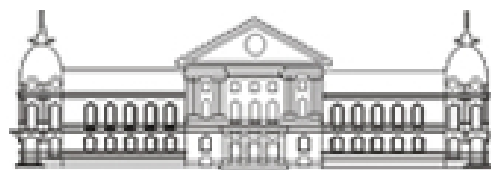


# ОСНОВИ НА МОДЕЛНОТО ПРЕДСКАЗВАЩО УПРАВЛЕНИЕ

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БЪЛГАРСКА  
АКАДЕМИЯ  
на НАУКИТЕ  
—1869—

# СЪДЪРЖАНИЕ

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1. Въведение в теорията на оптималното управление.
2. Линейно квадратично регулиране при наличие на ограничения.
3. Моделно предсказващо управление на линейни системи с ограничения.
4. Робастно моделно предсказващо управление на линейни системи при наличие на ограничени по амплитуда смущения.
5. Моделно предсказващо управление на система от втори ред.
6. Моделно предсказващо управление на лабораторен сепаратор.

# 1. Introduction to optimal control theory

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## General optimal control problem formulation (Ray, 1981)

System described by a set of non-linear, non-autonomous state equations:

$$\frac{dx}{dt} = f(x, u, t)$$

$x$  -  $n$ -dimensional vector of state variables

$u$  -  $m$ -dimensional vector of control variables

$f$  -  $n$ -dimensional vector function

$t$  - time

Initial state of the system:

$$x(0) = x_0$$

**Set of constraints:**

$$g(x, u) \geq 0$$

$$h(x, u) = 0$$

**Admissible range of control variables:**

$$u_{\min,i} \leq u_i \leq u_{\max,i} \quad , \quad i = 1, \dots, m$$

**Terminal constraint describing the target set:**

$$\psi[x(t_f)] \geq 0$$

**Performance index:**

$$I[u(t)] = G[x(t_f)] + \int_0^{t_f} F(x, u) dt \quad \rightarrow \quad \min$$

## Special cases:

- *minimum-time control problem*

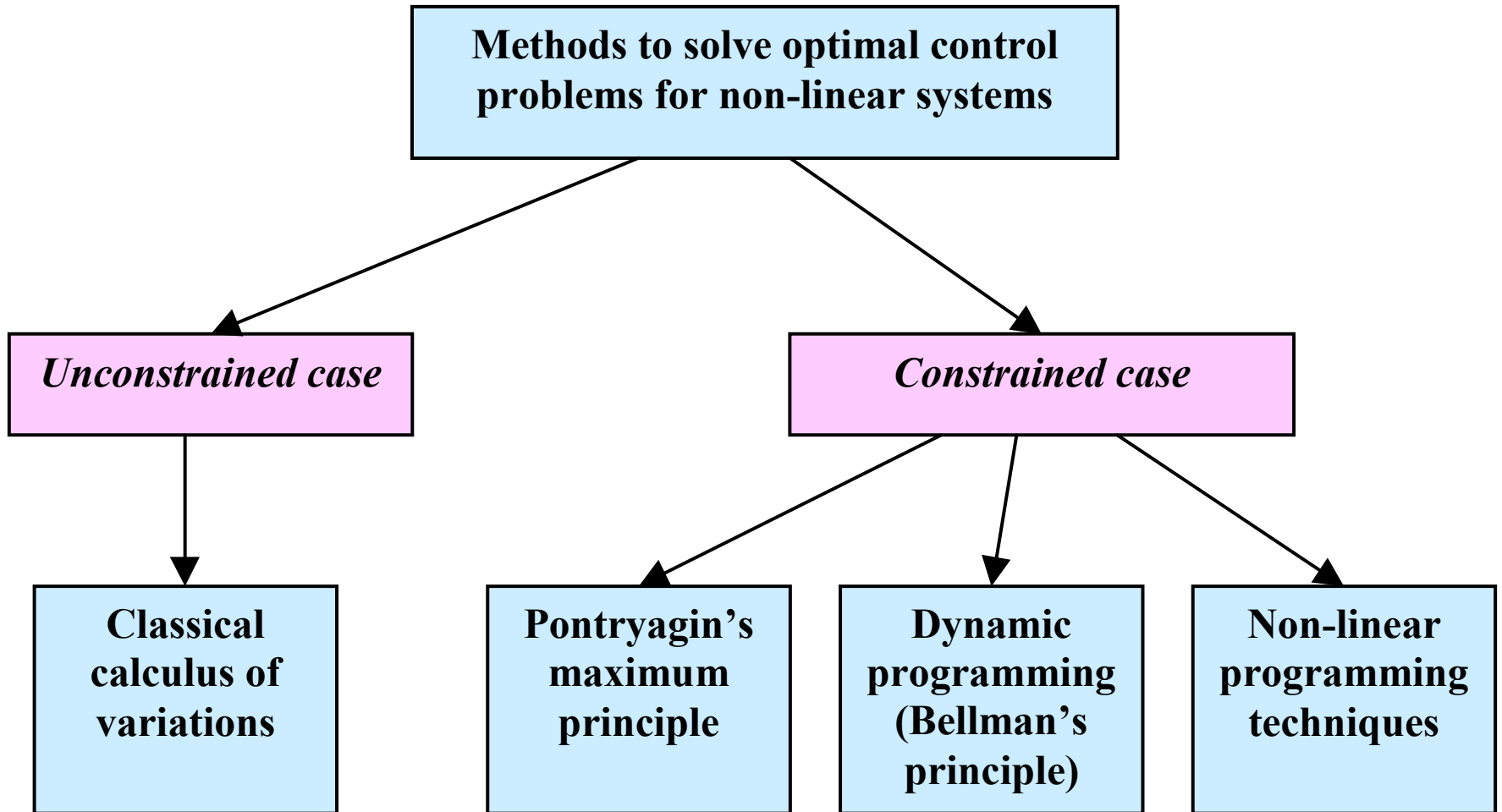
$$I[u(t)] = \int_0^{t_f} 1 dt \rightarrow \min$$

- *maximal productivity problem*

$$I[u(t)] = G[x(t_f)] \rightarrow \max$$

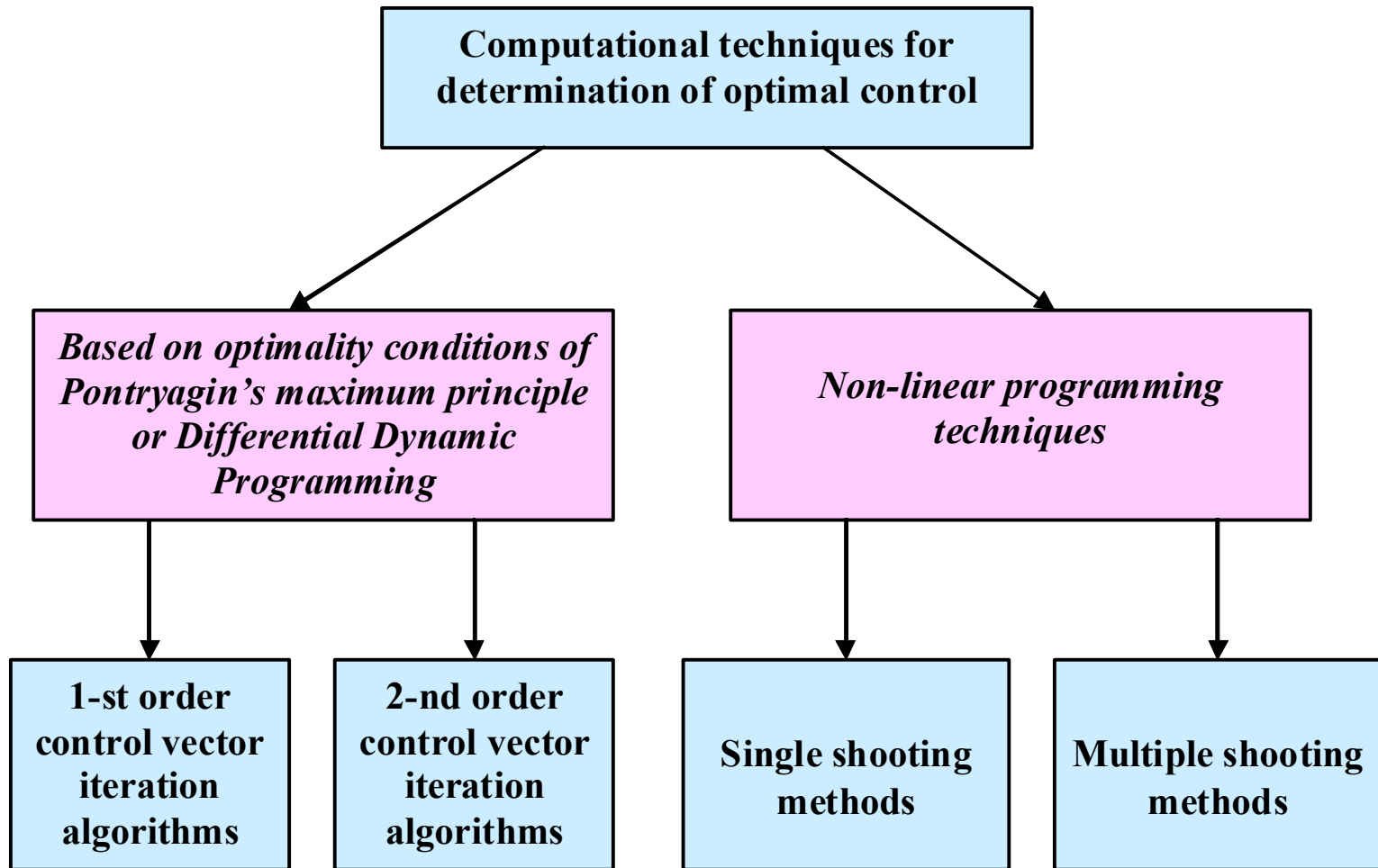
- *minimize an integral criterion*

$$I[u(t)] = \int_0^{t_f} F(x, u) dt \rightarrow \min$$



<b>Characteristics → Methods ↓</b>	<b>Takes into account presence of constraints</b>	<b>Mathematical model</b>	<b>Numerical difficulties</b>
<i>Classical calculus of variations</i>	No	continuous	TPBVP, stiffness
<i>Pontryagin's maximum principle</i>	Yes	continuous, discrete	TPBVP, stiffness
<i>Dynamic programming (Bellman's principle)</i>	Yes	continuous, discrete	curse of dimensionality
<i>Non-linear programming techniques</i>	Yes	continuous, discrete	high dimensional optimization problems

(Grancharova and Johansen, 2005)



(Grancharova and Johansen, 2005)



## Control vector iteration algorithms

(based on the optimality conditions of Pontryagin's maximum principle)

### 1 - st order methods :

(Ray, 1981)

$$u^{i+1}(t) = u^i(t) - \varepsilon \frac{\partial H}{\partial u}, \quad \varepsilon > 0, \quad t \in [0; t_f]$$

$$H = F(x, u) + \lambda^T f(x, u)$$

$$\frac{d\lambda}{dt} = -\frac{\partial H}{\partial x}, \quad \lambda_i(t_f) = \frac{\partial G}{\partial x_i}, \quad \text{for } x_i \text{ unspecified at } t_f$$

## 2 - nd order methods :

(Jacobson, 1968)

$$u^{i+1}(t) = u^i(t) - \left[ \frac{\partial^2 H}{\partial u^2} \right]^{-1} \left[ \varepsilon \left( \frac{\partial H}{\partial u} + \left( \frac{\partial f}{\partial u} \right)^T s \right) + \left( \frac{\partial^2 H}{\partial u \partial x} + \left( \frac{\partial f}{\partial u} \right)^T P \right) \delta x \right]$$

$$0 < \varepsilon \leq 1, t \in [0; t_f]$$

$$-\frac{ds}{dt} = \left( \frac{\partial f}{\partial x} \right)^T s - \left( \frac{\partial^2 H}{\partial u \partial x} + \left( \frac{\partial f}{\partial u} \right)^T P \right)^T \left[ \frac{\partial^2 H}{\partial u^2} \right]^{-1} \left( \frac{\partial H}{\partial u} + \left( \frac{\partial f}{\partial u} \right)^T s \right)$$

$$-\frac{dP}{dt} = \frac{\partial^2 H}{\partial x^2} + \left( \frac{\partial f}{\partial x} \right)^T P + P \frac{\partial f}{\partial x} - \left( \frac{\partial^2 H}{\partial u \partial x} + \left( \frac{\partial f}{\partial u} \right)^T P \right)^T \left[ \frac{\partial^2 H}{\partial u^2} \right]^{-1} \left( \frac{\partial^2 H}{\partial u \partial x} + \left( \frac{\partial f}{\partial u} \right)^T P \right)$$

with boundary conditions at  $t_f$ :  $P = \frac{\partial^2 G}{\partial x^2}$ ,  $s = 0$

## Single shooting methods:

control vector parameterization by a set of trial functions of time:

(Ray, 1981)

$$u_i(t) = \sum_{j=1}^l a_{ij} \phi_{ij}(t)$$

control vector parameterization by a set of trial functions of state:

(Ray, 1981)

$$u_i(t) = \sum_{j=1}^l b_{ij} \phi_{ij}(x)$$

## **Multiple shooting methods:**

(approximation of both control and state variables)

(Strand, 1989)

Parameters to be optimized:

$$P = [x_1(t_{ij}), x_2(t_{ij}), \dots, x_n(t_{ij}), u_1(t_j), u_2(t_j), \dots, u_m(t_j)]$$

$$j = 1, 2, \dots, M, \quad i = 1, 2, \dots, N_j, \quad t_{ij} \in [t^{j-1}; t^j]$$

## 2. Constrained linear quadratic regulation

(Scokaert and Rawlings, 1998)

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**Linear time-invariant discrete-time system:**

$$x(t+k+1) = Ax(t+k) + Bu(t+k) \quad , \quad k \geq 0$$

**Performance index:**

$$I[x(t), \{u(t), u(t+1), \dots\}] =$$

$$\sum_{k=0}^{\infty} [x^T(t+k)Qx(t+k) + u^T(t+k)Ru(t+k)]$$

**Constraints:**

$$Hx(t+k+1) \leq h \quad , \quad k \geq 0$$

$$Gu(t+k) \leq g \quad , \quad k \geq 0$$

# Problem 1 – Unconstrained linear quadratic regulation

$$\min_{\{u(t), u(t+1), \dots\}} \sum_{k=0}^{\infty} \left[ x^T(t+k) Q x(t+k) + u^T(t+k) R u(t+k) \right]$$

subject to:

$$x(t+k+1) = Ax(t+k) + Bu(t+k) , \quad k \geq 0$$

**Solution:**

$$u(t+k) = -Kx(t+k) , \quad k \geq 0$$

$$K = (B^T P B + R)^{-1} B^T P A$$

**Discrete-time algebraic Riccati equation:**

$$P = A^T P A - A^T P B (B^T P B + R)^{-1} (A^T P B)^T + Q$$

## Problem 2 - Constrained linear quadratic regulation:

$$\min_{\{u(t), u(t+1), \dots\}} \sum_{k=0}^{\infty} \left[ x^T(t+k) Q x(t+k) + u^T(t+k) R u(t+k) \right]$$

subject to:

$$x(t+k+1) = Ax(t+k) + Bu(t+k) , \quad k \geq 0$$

$$Hx(t+k+1) \leq h , \quad k \geq 0$$

$$Gu(t+k) \leq g , \quad k \geq 0$$

**difficulty** - infinite number of decision variables in the optimization  
and infinite number of constraints

## Problem 3 - Model Predictive Control (MPC) Problem:

$$\min_{\{u(t), u(t+1), \dots, u(t+N-1)\}} \sum_{k=0}^{N-1} \left[ x^T(t+k) Q x(t+k) + u^T(t+k) R u(t+k) \right]$$

subject to:

$$x(t+k+1) = Ax(t+k) + Bu(t+k) \quad , \quad k \geq 0$$

$$Hx(t+k+1) \leq h \quad , \quad k = 0, 1, \dots, N-1$$

$$Gu(t+k) \leq g \quad , \quad k = 0, 1, \dots, N-1$$

$$u(t+k) = -Kx(t+k) \quad , \quad k \geq N$$

- finite number of decision variables,  $Nm$ , and finite number of constraints  $N(n_h + n_g)$ ;
- it can be solved with standard quadratic programming methods



- **The finite-horizon optimization (Model Predictive Control) also provides the solution to the infinite-horizon linear quadratic regulation problem with constraints (Sznaier and Damborg, 1987)**
- For any given compact set of initial conditions, the algorithm in (Chmielewski and Manousiouthakis, 1996) provides **the horizon  $N$**  such that the **MPC controller** (solution of Problem 3) **solves the infinite horizon problem** (Problem 2)

# Implicit approach to constrained linear quadratic regulation

*implicit* - the optimal control does not have the form of feedback control law, but it is obtained in the form of open-loop time trajectory

## **Definition:**

Let  $X_K \subseteq R^n$  denotes the set of states  $x(t)$  for which the unconstrained LQR law,  $u(t + k) = -Kx(t + k)$ ,  $k \geq 0$ , satisfies all constraints.

***Control Algorithm (Scokaert and Rawlings, 1998):***

**0).** Choose a finite horizon  $N_0$ , set  $N = N_0$ .

**1).** Solve *Problem 3 (MPC problem)*.

**2).** If  $x(t + N) \in X_K$ , go to step 4).

**3).** Increase  $N$ , go to step 1).

**4).** Terminate:  $\pi^* = \pi_N$ .

$\pi_N = [u(t), u(t+1), \dots, u(t+N-1)]$  – the optimal control trajectory determined by solving the MPC problem

$\pi^*$  – the optimal control trajectory that is a solution of the constrained LQR problem

# 3. Model Predictive Control of Constrained Linear Systems

## ▪ MPC problem formulation

(Mayne et al., 2000; Bemporad et al., 2002)

Consider the problem of regulating to the origin the discrete-time linear time invariant system:

$$x(t+1) = Ax(t) + Bu(t) \tag{1}$$

$$y(t) = Cx(t)$$

while satisfying the following constraints:

$$y_{\min} \leq y(t) \leq y_{\max} \tag{2}$$

$$u_{\min} \leq u(t) \leq u_{\max} \tag{3}$$

# Model Predictive Control (MPC) solves the problem in the following way:

Assume that a full measurement of the state  $x(t)$  is available at the current time  $t$ . Then, the optimization problem:

$$\min_{U \equiv \{u_t, u_{t+1}, \dots, u_{t+N_u-1}\}} \left\{ \begin{array}{l} I[U, x(t)] = x_{t+N_y|t}^T P x_{t+N_y|t} + \\ \sum_{k=0}^{N_y-1} \left[ x_{t+k|t}^T Q x_{t+k|t} + u_{t+k}^T R u_{t+k} \right] \end{array} \right\} \quad (4)$$

subject to:

$$x_{t|t} = x(t)$$

$$y_{\min} \leq y_{t+k|t} \leq y_{\max} \quad , \quad k = 1, \dots, N_c$$

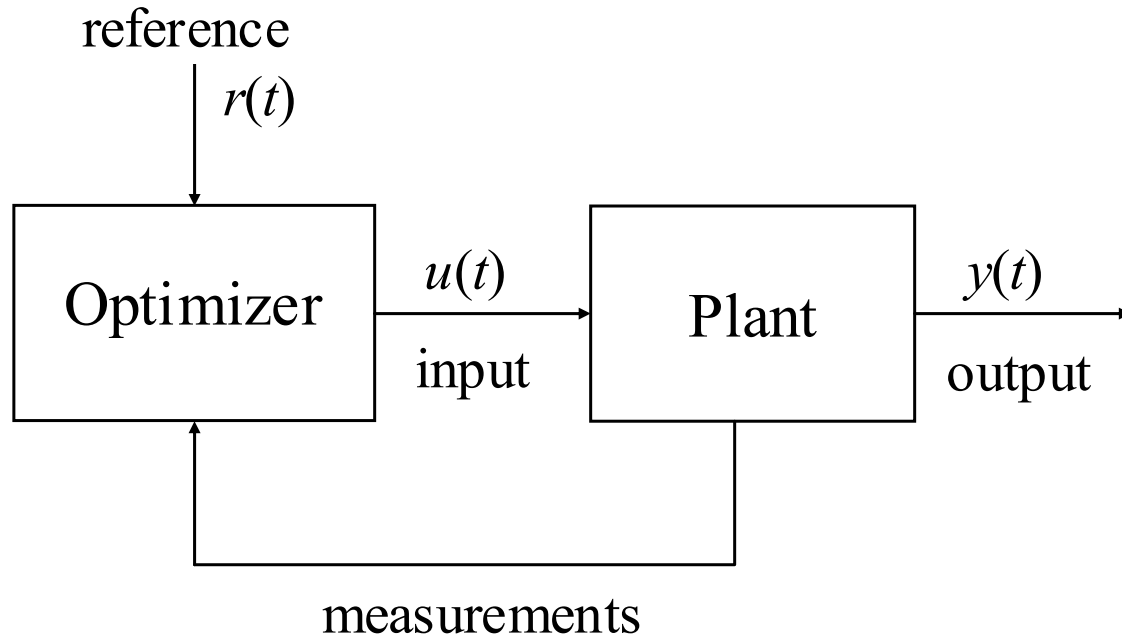
$$u_{\min} \leq u_{t+k} \leq u_{\max} \quad , \quad k = 0, 1, \dots, N_c$$

$$x_{t+k+1|t} = Ax_{t+k|t} + Bu_{t+k} \quad , \quad k \geq 0$$

$$y_{t+k|t} = Cx_{t+k|t} \quad , \quad k \geq 0$$

$$u_{t+k} = -Kx_{t+k|t} \quad , \quad N_u \leq k < N_y$$

is solved at each time  $t$ .



$N_y$  - output horizon (prediction horizon)

$N_u$  - input horizon

$N_c$  - constraints horizon

$$N_u \leq N_y, \quad N_c \leq N_y - 1$$

1). Choose  $K=0$  and  $P$  as the solution of the Lyapunov equation:

$$P = A^T P A + Q \quad (5)$$

2). Set  $K=K_{LQ}$ , where  $K_{LQ}$  and  $P$  are the solution of the unconstrained infinite horizon LQR problem with weights  $Q$  and  $R$ :

$$K_{LQ} = \left( R + B^T P B \right)^{-1} B^T P A \quad (6)$$

$$P = \left( A + B K_{LQ} \right)^T P \left( A + B K_{LQ} \right) + K_{LQ}^T R K_{LQ} + Q$$



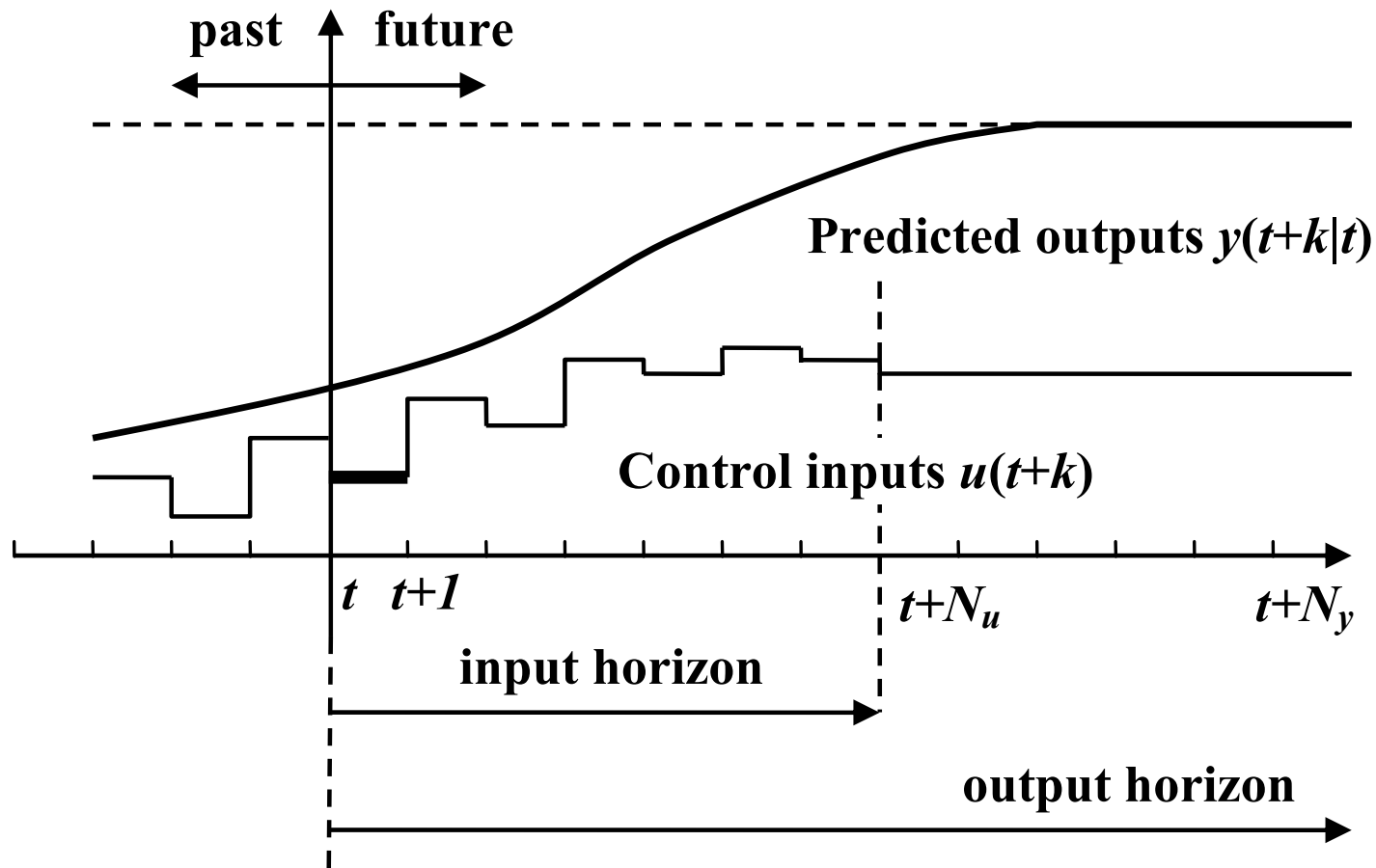
## Moving (receding horizon) strategy:

At time  $t$  compute the optimal solution  
(the optimal input sequence):

$$U^*(t) = [u_t^*, \dots, u_{t+N_u-1}^*]$$

and apply to the system **only the first input** from the sequence:

$$u(t) = u_t^* \tag{7}$$



**Receding horizon strategy:** only the first input of the computed optimal input sequence is implemented

- **Stability**

## Theorem (Bemporad et al., 2002):

Let  $N_y = \infty$ ,  $K = 0$  or  $K = K_{LQ}$ , and  $N_c < \infty$  be sufficiently large for guaranteeing existence of feasible input sequences at each time step. Then the MPC law (4) - (7) asymptotically stabilizes system (1) while enforcing the fulfillment of the constraints (2) - (3) from all initial states  $x(0)$  such that the optimization problem (4) is feasible at  $t = 0$ .

(For more details about stability, see (Mayne et al., 2000))

## ■ MPC computation

By substituting:

$$x_{t+k|t} = A^k x(t) + \sum_{j=0}^{k-1} A^j B u_{t+k-1-j}$$

the optimization problem becomes:

$$V[x(t)] = \frac{1}{2} x^T(t) Y x(t) + \min_U \left\{ \frac{1}{2} U^T H U + x^T(t) F U \right\}$$

subject to:

$$G U \leq W + E x(t)$$

**Quadratic Programming  
problem**

$U \equiv [u_t^T, \dots, u_{t+N_u-1}^T]^T \in R^s$  ,  $s = m N_u$  – the optimization vector

# 4. Robust Model Predictive Control of Constrained Linear Systems With Bounded Disturbances

(Grancharova and Johansen, 2005)

Linear system with  
*disturbance input:*

$$\begin{aligned} \mathbf{x}(t+1) &= \mathbf{A}\mathbf{x}(t) + \mathbf{B}u(t) + \mathbf{T}\boldsymbol{\theta}(t), \boldsymbol{\theta}(t) \in \Theta^A \subset \mathbf{R}^s \\ \mathbf{y}(t) &= \mathbf{C}\mathbf{x}(t) \end{aligned}$$

Disturbance realization:

$$\begin{aligned} \Theta &\equiv [\boldsymbol{\theta}_t^T, \dots, \boldsymbol{\theta}_{t+N-1}^T]^T \in \Theta^B \\ \Theta &\in \Theta^B = \{\Theta^A \times \Theta^A \dots \times \Theta^A\} \subset \mathbf{R}^{sN} \end{aligned}$$

Optimization problem:

$$V^*(x(t), \Theta) = \min_{U \equiv \{u_t, \dots, u_{t+N-1}\}} J(U, x(t), \Theta)$$

Constraints:

$$\begin{aligned} u_{\min} &\leq u_{t+k} \leq u_{\max}, \quad k = 0, 1, \dots, N-1 \\ y_{\min} &\leq y_{t+k|t} \leq y_{\max}, \quad k = 1, \dots, N \end{aligned}$$

Cost function:

$$J(U, x(t), \Theta) = \sum_{k=0}^{N-1} \left[ x_{t+k|t}^T Q x_{t+k|t} + u_{t+k}^T R u_{t+k} \right] + x_{t+N|t}^T P x_{t+N|t}$$

Nominal optimization criterion:

$$V_{nom}^*(x(t)) = \min_{U \equiv \{u_t, \dots, u_{t+N-1}\}} J(U, x(t), \theta^N)$$

Nominal value  
of the disturbance input:

$$\theta(t) = \theta^N = 0$$

## Robustness:

Satisfaction of the output and input constraints under *all possible disturbance realizations*  $\Theta \in \Theta^B$

The robust MPC can be represented as a QP problem:

$$V_{z,nom}^*(\mathbf{x}) = \min_z \frac{1}{2} \mathbf{z}^T \mathbf{H} \mathbf{z}$$

subject to :  $\mathbf{G} \mathbf{z} \leq \mathbf{W} + \mathbf{S}_1 \mathbf{x}(t) + \mathbf{S}_2 \Theta, \forall \Theta \in \Theta^B$

Optimization variables:

$$\mathbf{z} \equiv \mathbf{U} + \mathbf{H}^{-1} \mathbf{F}^T \mathbf{x}(t), \mathbf{U} \equiv [\mathbf{u}_t^T, \dots, \mathbf{u}_{t+N-1}^T]^T$$



## Assumption:

The disturbance input set  $\Theta^A = \{ \theta \in \mathbf{R}^s \mid \theta^L \leq \theta \leq \theta^U \}$  represents a hyper-rectangle that includes the origin in its interior.

## Definition:

Consider the  $i$ -th constraint defined by  $G^i, W^i, S_1^i, S_2^i$  rows of the matrices  $G, W, S_1, S_2$ . The worst disturbance realization for the  $i$ -th constraint, denoted by  $\tilde{\Theta}^i \in \Theta^B$ , is one which solves the linear program:

$$S_2^i \tilde{\Theta}^i = \min_{\Theta \in \Theta^B} \{ S_2^i \Theta \}$$

**Lemma:**

*If there exist a  $\mathbf{z}$  that satisfies the following constraint:*

$$\mathbf{G}\mathbf{z} \leq \tilde{\mathbf{W}} + \mathbf{S}_1\mathbf{x}(t),$$

*where the  $i$ -th row of the matrix  $\tilde{\mathbf{W}}$  is determined by:*

$$\tilde{W}^i = W^i + \mathbf{S}_2^i \tilde{\Theta}^i,$$

*and where  $\tilde{\Theta}^i \in \Theta^B$  is the worst disturbance realization for the  $i$ -th constraint, then this implies that  $\mathbf{z}$  will satisfy the constraint*

$\mathbf{G}\mathbf{z} \leq \mathbf{W} + \mathbf{S}_1\mathbf{x}(t) + \mathbf{S}_2\Theta$  *for all possible disturbance realizations*

$\Theta \in \Theta^B$  . *Such a control is referred to as **robustly feasible**.*

**Equivalent QP problem without disturbance:**

$$V_{z,nom}^*(\mathbf{x}) = \min_z \frac{1}{2} \mathbf{z}^T \mathbf{H} \mathbf{z}$$

subject to:

$$\mathbf{G} \mathbf{z} \leq \tilde{\mathbf{W}} + \mathbf{S}_1 \mathbf{x}(t)$$

# 5. Model Predictive Control of a Second-Order System

- **absence of disturbance**

$$x(t+1) = Ax(t) + Bu(t)$$

$$A = \begin{bmatrix} 1 & T_s \\ 0 & 1 \end{bmatrix}, \quad B = \begin{bmatrix} T_s^2 \\ T_s \end{bmatrix}$$

Sampling time  $T_s=0.05$  [s]

$$N = 2, \quad Q = \begin{bmatrix} 1 & 0 \\ 0 & 0 \end{bmatrix}, \quad R = 1$$

$$\begin{array}{l} \text{Constraints :} \\ -1 \leq u \leq 1 \\ -0.5 \leq x_2 \leq 0.5 \end{array}$$

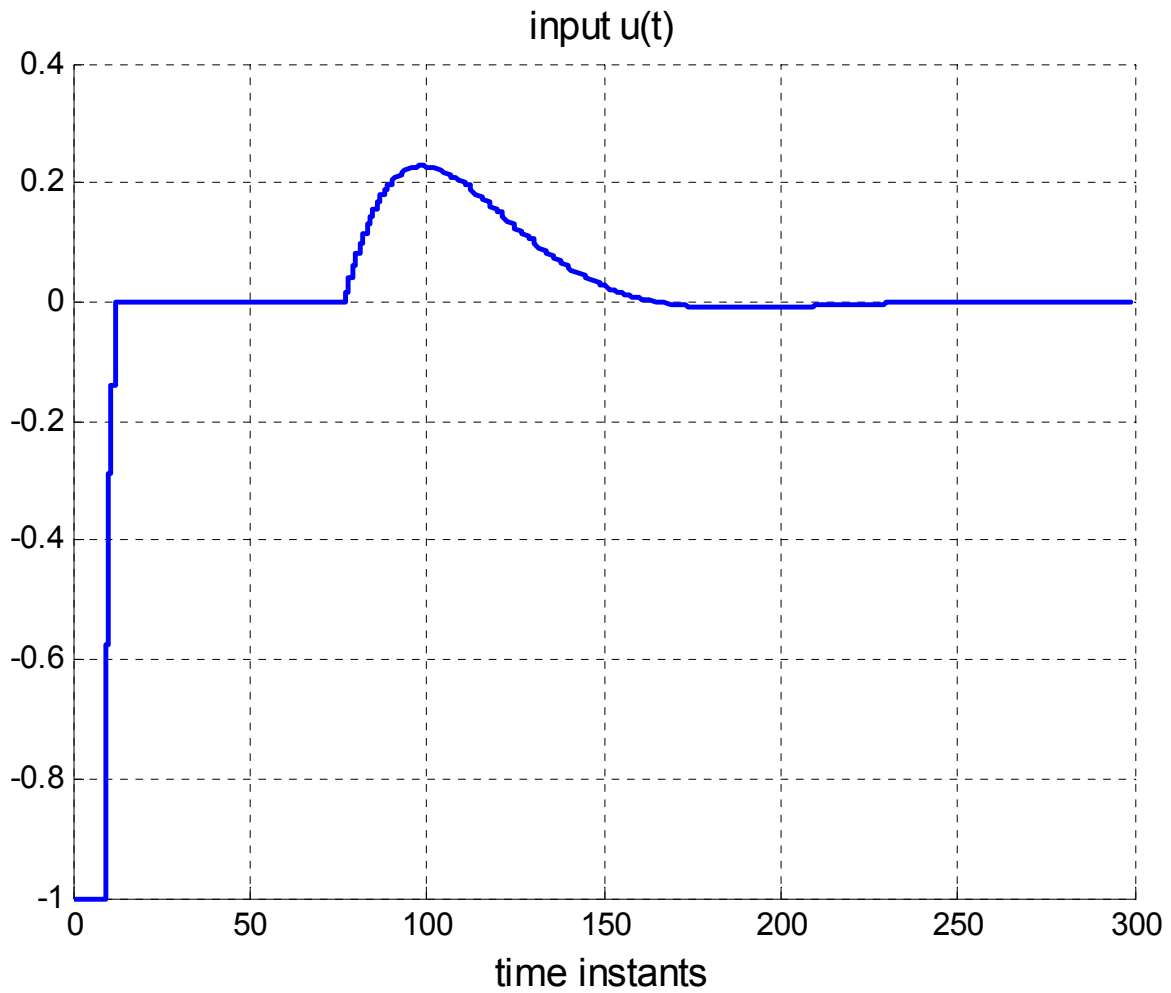
## Matrices in the QP problem:

$$H = \begin{bmatrix} 2.157 & 0.152 \\ 0.152 & 2.147 \end{bmatrix} \quad F = \begin{bmatrix} 2.218 & 2.072 \\ 3.146 & 3.035 \end{bmatrix}$$

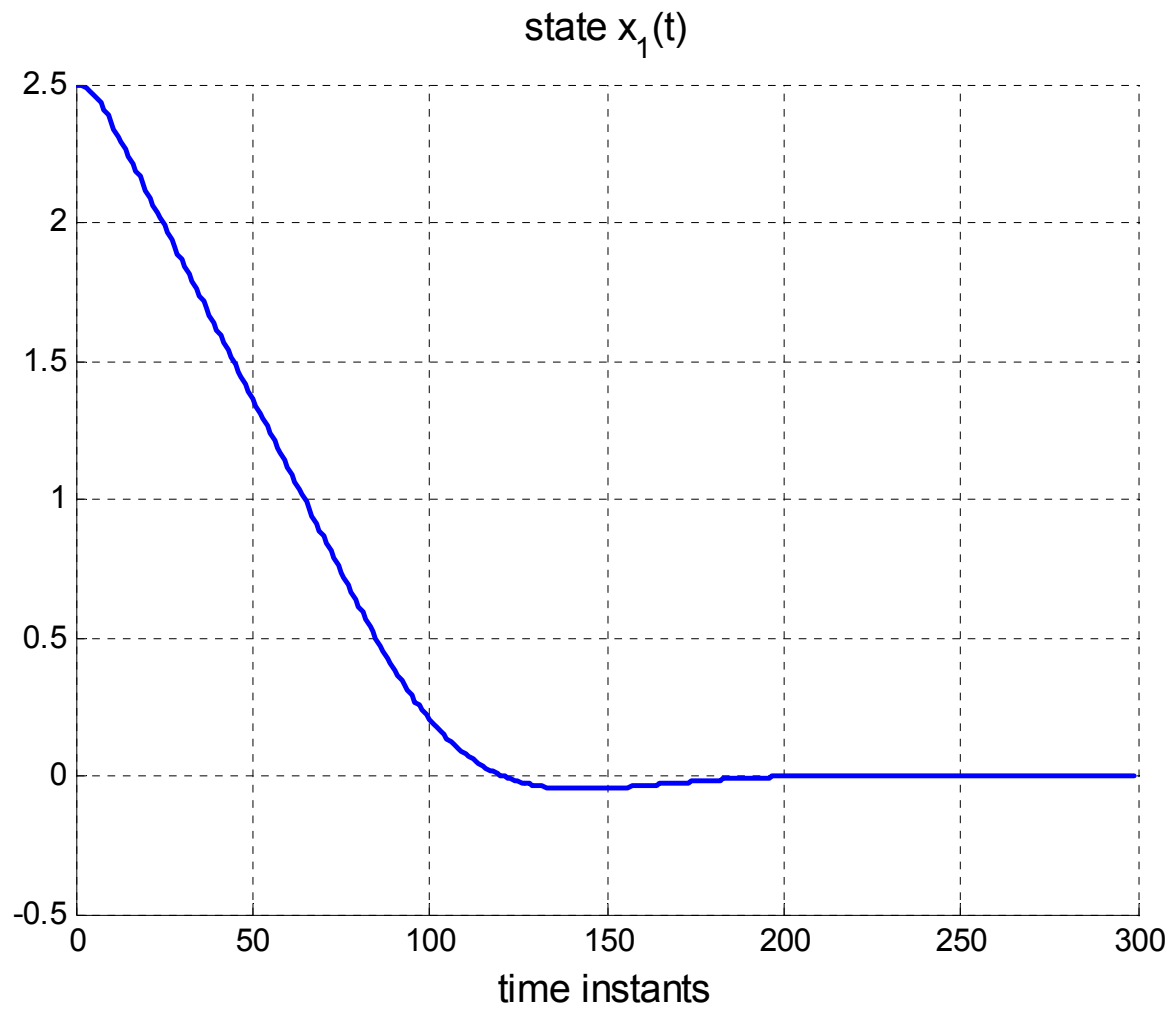
$$G = \begin{bmatrix} -1 & 0 \\ 0 & -1 \\ 1 & 0 \\ 0 & 1 \\ -0.05 & 0 \\ -0.05 & -0.05 \\ 0.05 & 0 \\ 0.05 & 0.05 \end{bmatrix}$$

$$W = \begin{bmatrix} 1 \\ 1 \\ 1 \\ 1 \\ 0.5 \\ 0.5 \\ 0.5 \\ 0.5 \end{bmatrix}$$

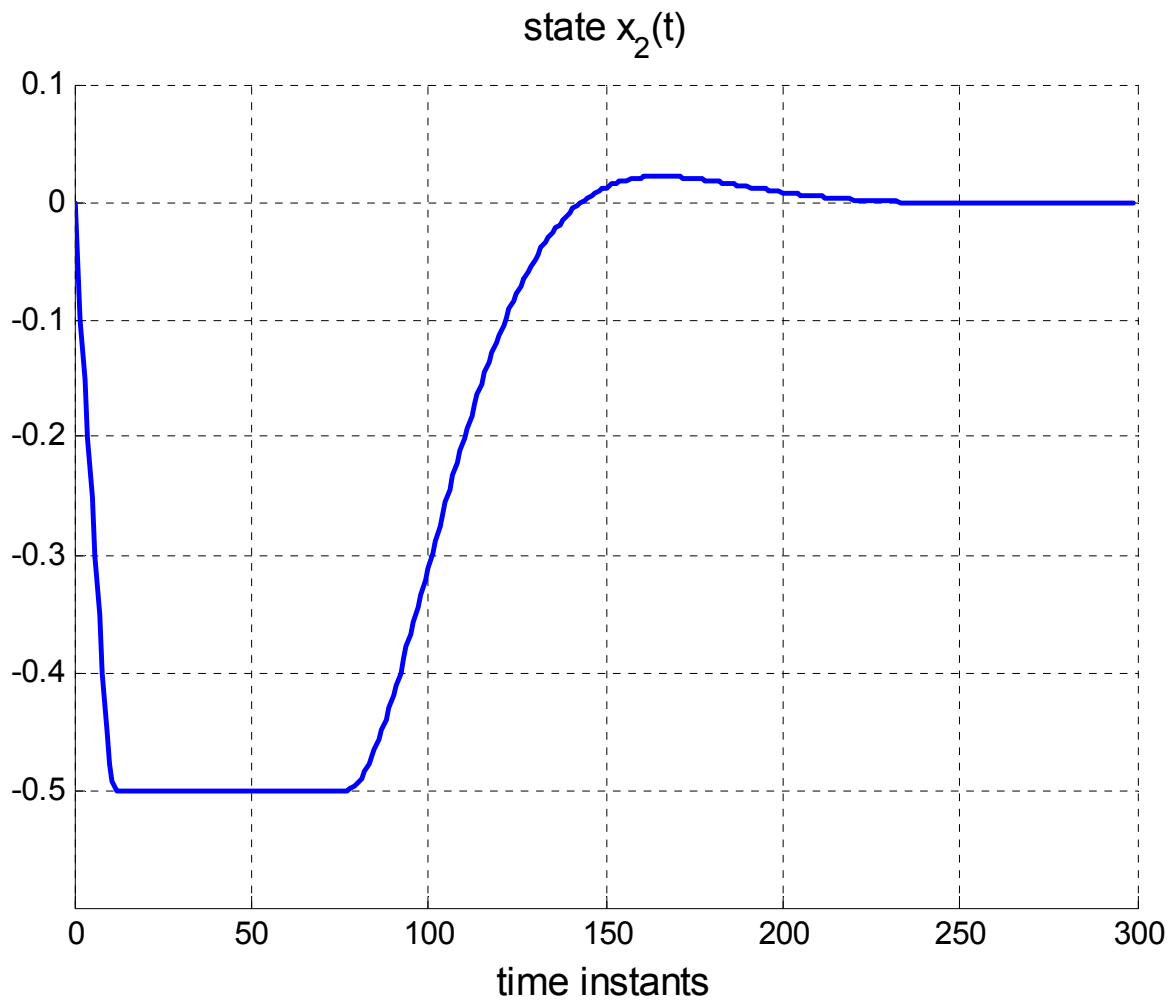
$$E = \begin{bmatrix} 0 & 0 \\ 0 & 0 \\ 0 & 0 \\ 0 & 0 \\ 0 & 1 \\ 0 & 1 \\ 0 & -1 \\ 0 & -1 \end{bmatrix}$$



Optimal control input trajectory



Optimal trajectory of  $x_1$



Optimal trajectory of  $x_2$



▪ **presence of disturbance**

$$x(t+1) = Ax(t) + Bu(t) + T\theta(t)$$

$$A = \begin{bmatrix} 1 & T_s \\ 0 & 1 \end{bmatrix}, \quad B = \begin{bmatrix} T_s^2 \\ T_s \end{bmatrix}, \quad T = \begin{bmatrix} 1 & 0 \\ 0 & 1 \end{bmatrix}$$

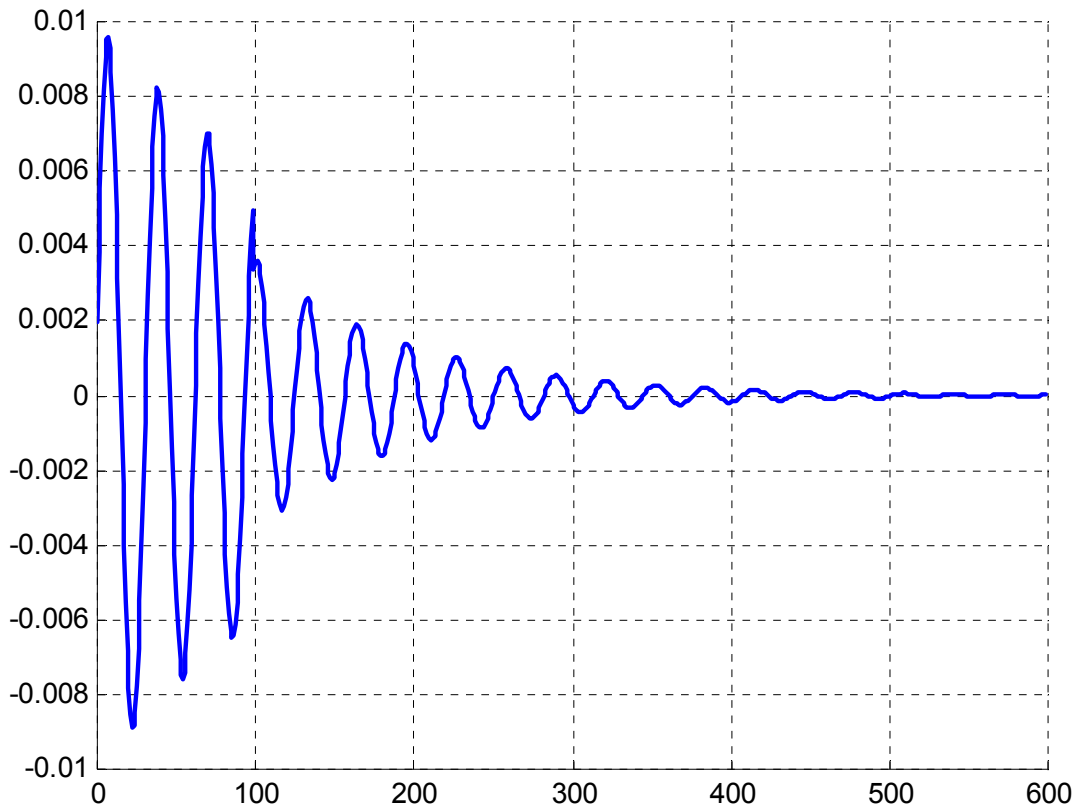
$$N = 5, \quad Q = \begin{bmatrix} 1 & 0 \\ 0 & 0 \end{bmatrix}, \quad R = 1$$

$$\begin{array}{l} \text{Constraints :} \\ -1 \leq u \leq 1 \\ -0.5 \leq x_2 \leq 0.5 \end{array}$$

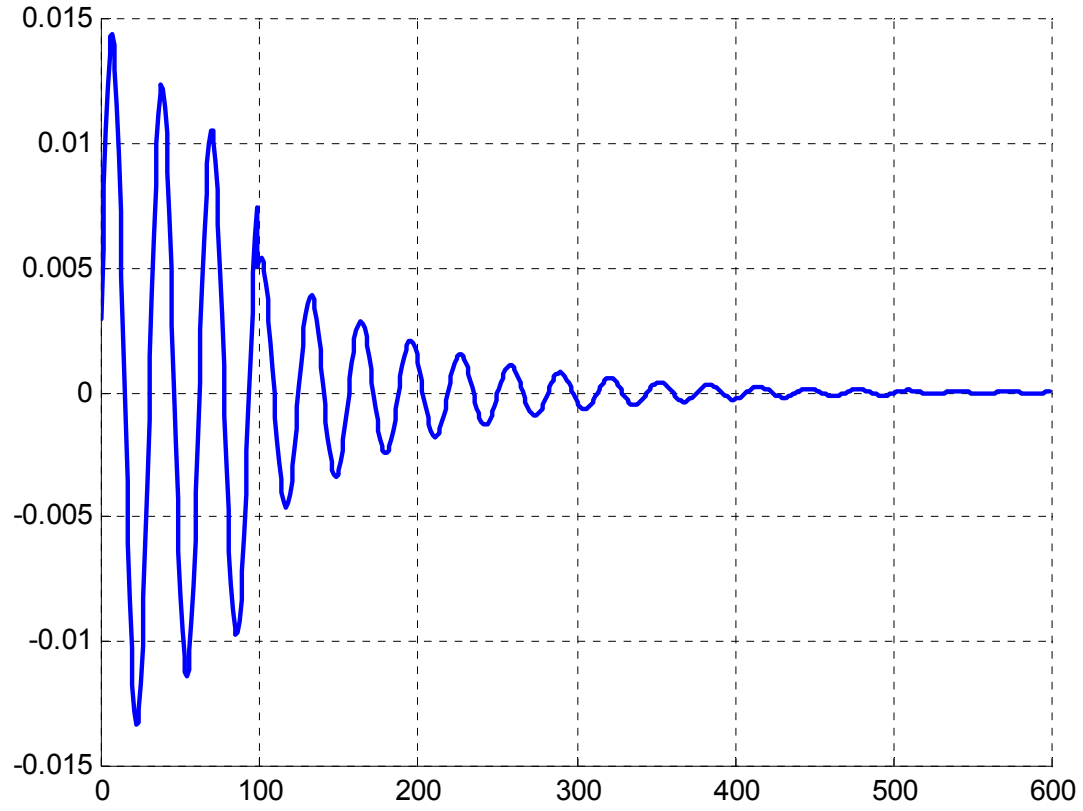
Disturbances have the following bounds:

$$-0.01 \leq \theta_1(t) \leq 0.01$$

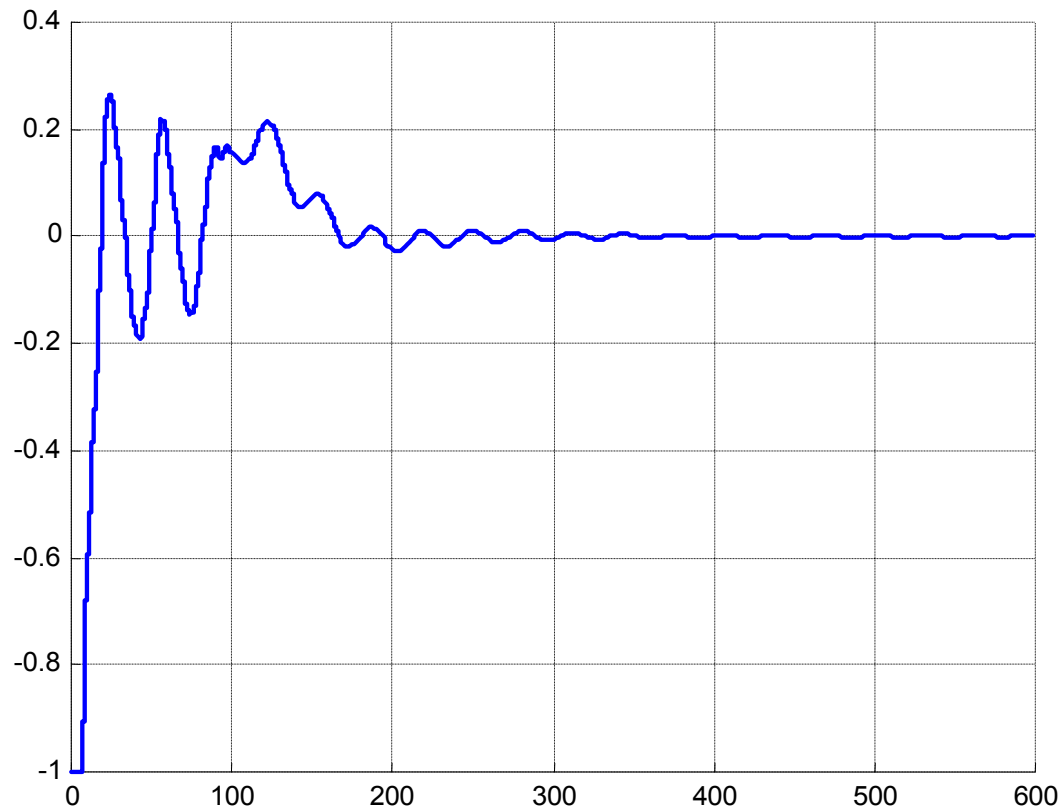
$$-0.015 \leq \theta_2(t) \leq 0.015$$



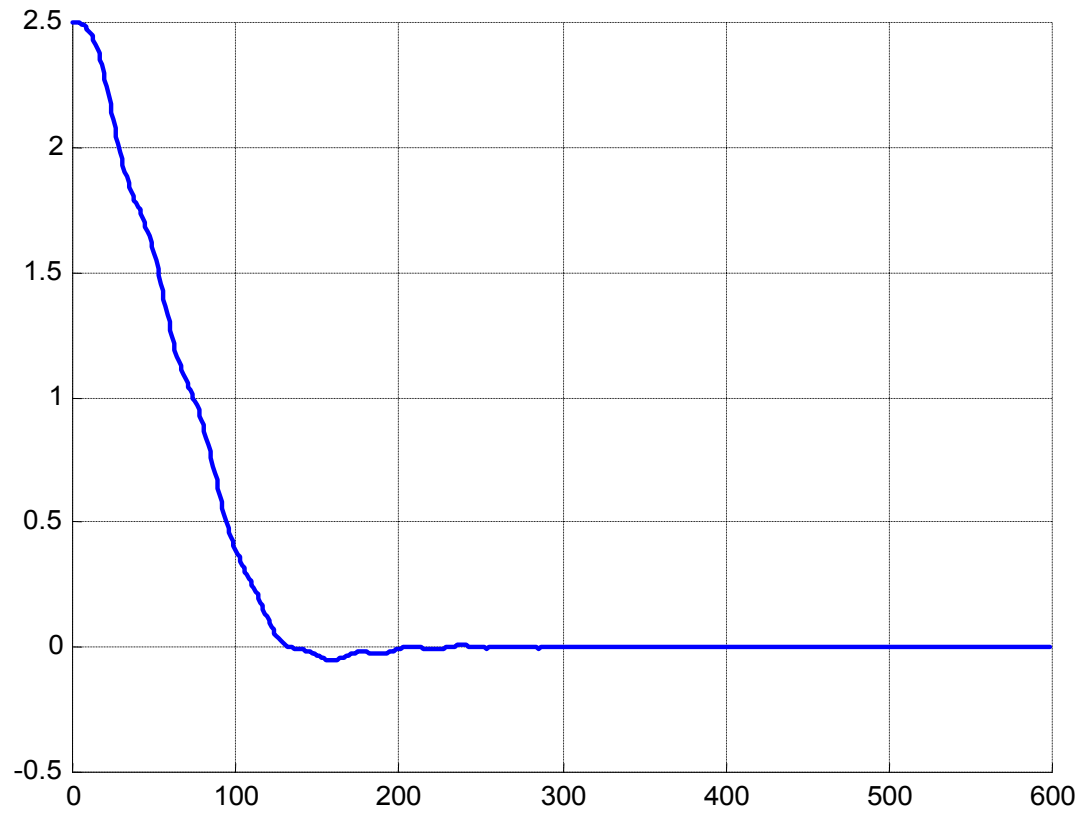
Disturbance  $\theta_1(t)$



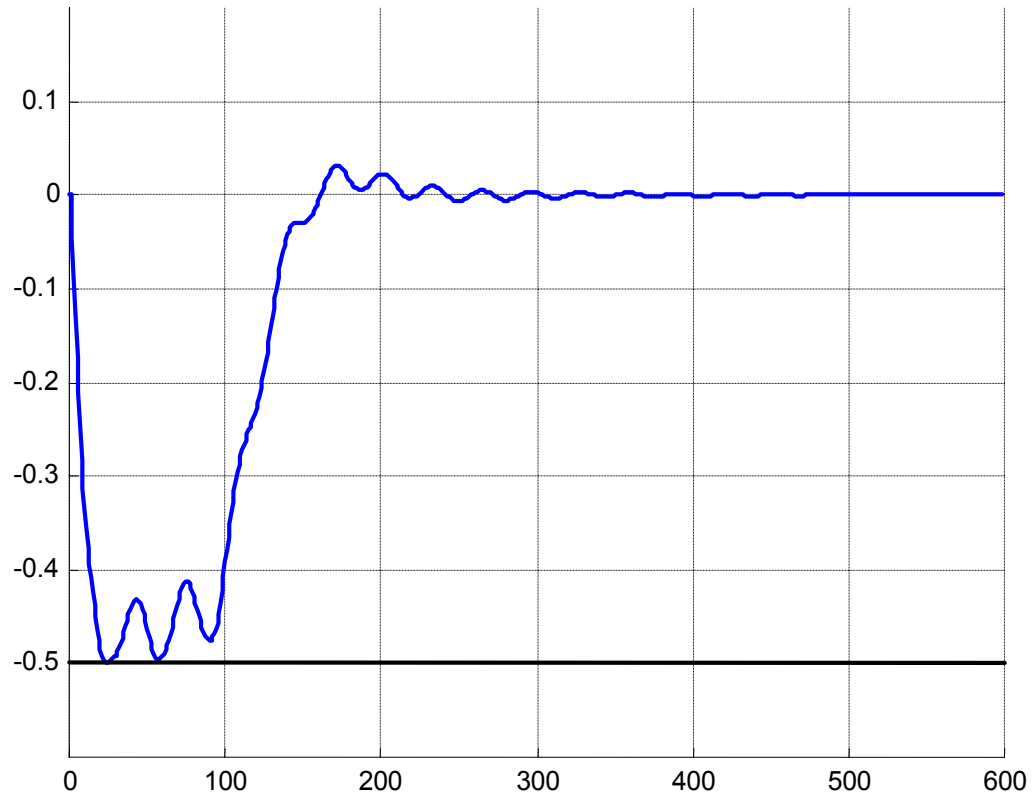
Disturbance  $\theta_2(t)$



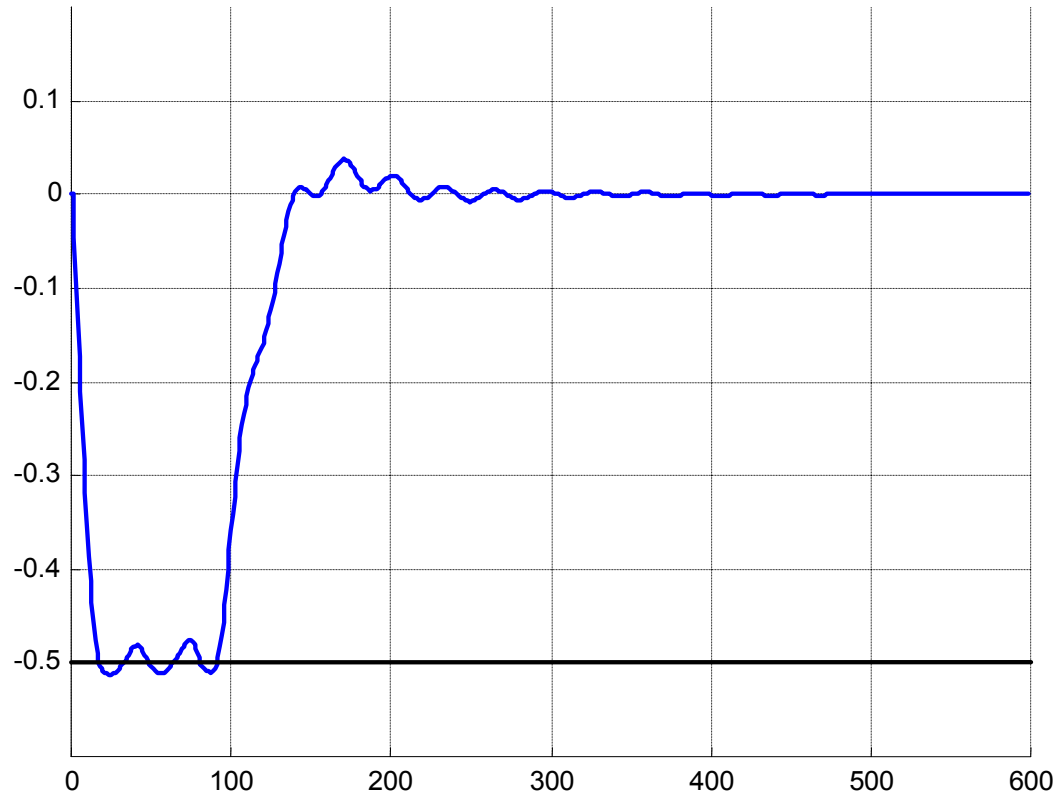
Control input trajectory with the robust MPC



State  $x_1$  trajectory with the robust MPC



State  $x_2$  trajectory with the robust MPC



State  $x_2$  trajectory with the nominal MPC

# 6. Model Predictive Control of a Laboratory Separator

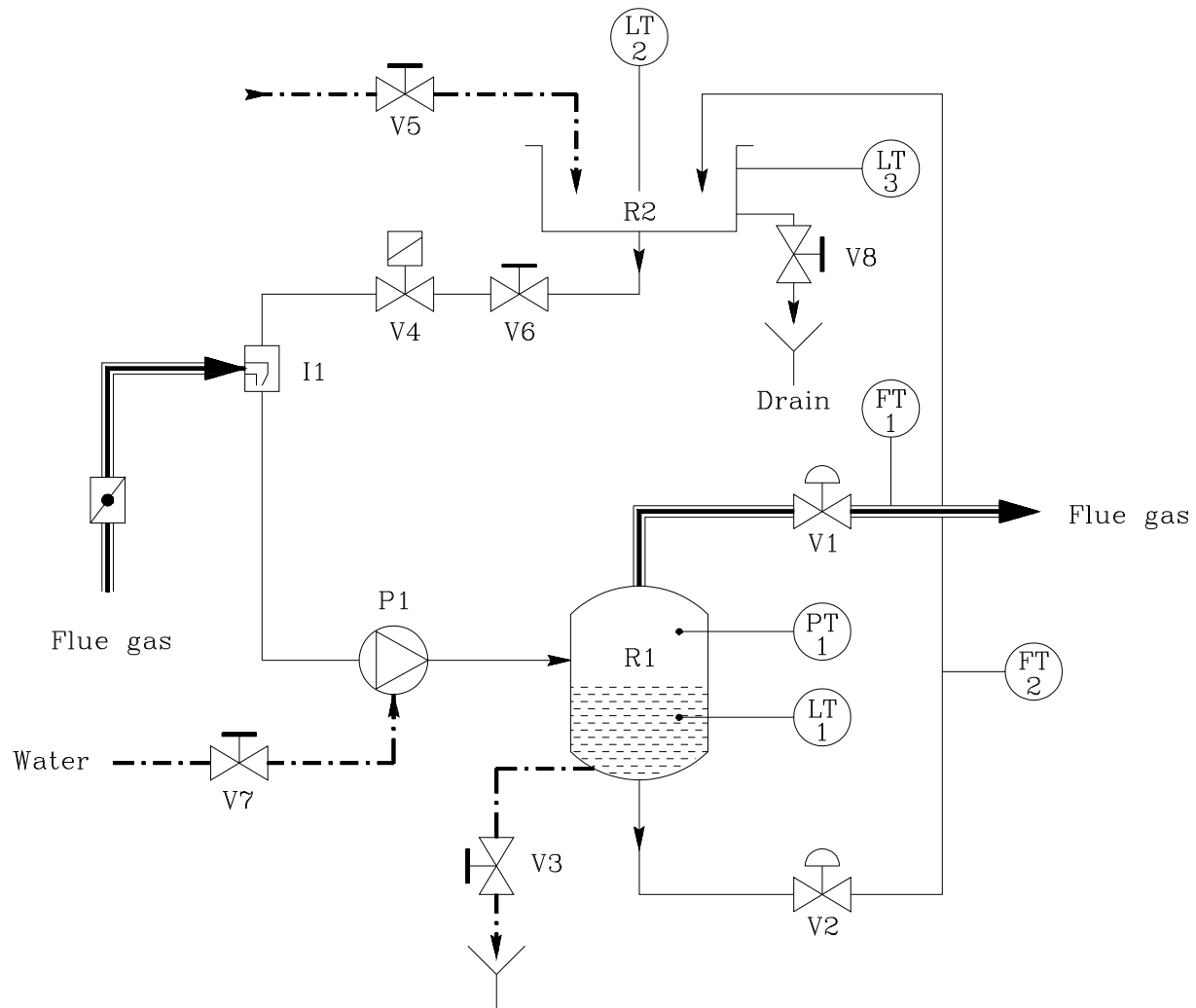
(Grancharova, Johansen, and Kocijan, 2004)

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Pilot installation at Jozef Stefan Institute, Slovenia





Gas-liquid separator (Vrančić et al., 1995)

## Process model: (Vrančić et al., 1995)

$$\text{Valve } V_1 \left\{ \begin{array}{l} K_1 = K_{01} \cdot R_{V1}^{v_1-1} = 75.1 \cdot 46.1^{v_1-1} \text{ [l/(s}\sqrt{\text{bar)}}] \\ v_1 = \begin{cases} 1 & \text{if } r_1 > 1 \\ 0 & \text{if } r_1 < 0 \\ r_1 & \text{otherwise} \end{cases} \end{array} \right.$$

$$\text{Valve } V_2 \left\{ \begin{array}{l} K_2 = K_{02} \cdot R_{V2}^{v_2-1} = 0.742 \cdot 75.66^{v_2-1} \text{ [l/(s}\sqrt{\text{bar)}}] \\ v_2 = \begin{cases} r_{2\max} & \text{if } r_2 > r_{2\max} \\ 0 & \text{if } r_2 < 0 \\ r_2 & \text{otherwise} \end{cases} \\ r_{2\max} = 0.8625 \end{array} \right.$$

## Speed limit of valves positions:

$$\dot{v} = \begin{cases} \dot{v}_{\max} & \text{if } \dot{r} > \dot{v}_{\max} \\ \dot{v}_{\min} & \text{if } \dot{r} < \dot{v}_{\min} \\ \dot{r} & \text{otherwise} \end{cases}$$

$$\dot{v}_{\max} = 0.66 [\text{s}^{-1}]$$

$$\dot{v}_{\min} = -0.33 [\text{s}^{-1}]$$

Air flow through valve  $V_1$ :

$$\Phi_1 = K_1 \sqrt{p_1} \text{ [l/s]}$$

Water flow through valve  $V_2$ :

$$\Phi_2 = K_2 \sqrt{p_1 + K_W (h_1 - h_{R2})} \text{ [l/s]}$$

Water flow to the separator  $R_1$ :

$$\Phi_w = 0.1644 \text{ [l/s]}$$

Air flow to the separator  $R_1$ :

$$\Phi_{air} = \Phi_{air0} + \Phi_{air1} \cdot p_1 = 6.46 - 1.615 \cdot p_1 \text{ [l/s]}$$

The change of water level in  $R_1$ :

$$\frac{dh_1}{dt} = \frac{1}{S_1} (\Phi_w - \Phi_2) K_F \text{ [m/s]}$$

The change of water level in  $R_2$ :

$$\frac{dh_2}{dt} = \frac{1}{S_2} (\Phi_2 - \Phi_w) K_F \text{ [m/s]}$$

The change of air pressure inside  $R_1$ :

$$\frac{dp_1}{dt} = \frac{1}{V} [p_0 (\Phi_{air} - \Phi_1) K_F + (p_0 + p_1) (\Phi_w - \Phi_2) K_F] \text{ [bar/s]}$$

The air volume inside  $R_1$ :

$$V = S_1 (h_{R1} - h_1) = S_1 (2.25 - h_1) \text{ [m}^3\text{]}$$

# Linearized model of the gas-liquid separation plant

$$\begin{bmatrix} \Delta \dot{p}_1 \\ \Delta \dot{h}_1 \end{bmatrix} = A_c \begin{bmatrix} \Delta p_1 \\ \Delta h_1 \end{bmatrix} + B_c \begin{bmatrix} \Delta v_1 \\ \Delta v_2 \end{bmatrix}$$

$\Delta p_1 = p_1 - p_{1s}$  - change of pressure from the steady state;

$\Delta h_1 = h_1 - h_{1s}$  - change of liquid level;

$\Delta v_1 = v_1 - v_{1s}$  - change of position of Valve 1;

$\Delta v_2 = v_2 - v_{2s}$  - change of position of Valve 2;

## Elements of $A_c$ : (Vrančić et al., 1995)

$$a_{11} = \frac{K_F}{V_s} \left[ p_0 \left( \Phi_{air1} - \frac{K_{1s}}{2\sqrt{p_{1s}}} \right) - (p_0 + p_{1s}) \frac{K_{2s}}{2\sqrt{p_{V2s}}} \right]$$

$$a_{12} = -\frac{K_F}{V_s} \left[ (p_0 + p_{1s}) \frac{K_{2s} K_w}{2\sqrt{p_{V2s}}} \right]$$

$$a_{21} = -\frac{K_F}{S_1} \left[ \frac{K_{2s}}{2\sqrt{p_{V2s}}} \right]$$

$$a_{22} = -\frac{K_F}{S_1} \left[ \frac{K_{2s} K_w}{2\sqrt{p_{V2s}}} \right]$$

## Elements of $B_c$ : (Vrančić et al., 1995)

$$b_{11} = -\frac{K_F}{V_s} p_0 K_{1s} \sqrt{p_{1s}} \ln(R_{V1})$$

$$b_{12} = -\frac{K_F}{V_s} (p_0 + p_{1s}) K_{2s} \sqrt{p_{V2s}} \ln(R_{V2})$$

$$b_{21} = 0$$

$$b_{22} = -\frac{K_F}{S_1} K_{2s} \sqrt{p_{V2s}} \ln(R_{V2})$$



## Linear continuous-time model:

$$A_c = \begin{bmatrix} -0.0285 & -0.0001 \\ -0.0006 & -0.0001 \end{bmatrix}, \quad B_c = \begin{bmatrix} -0.0843 & -0.0041 \\ 0 & -0.0023 \end{bmatrix}$$

corresponding to steady state:

$$p_{1s} = 0.5 \text{ bar}, \quad h_{1s} = 1.4 \text{ m}, \quad v_{1s} = 0.4152, \quad v_{2s} = 0.7462$$

## Linear discrete-time model:

- sampling time  $T_s=1$ sec
- steady state:

$$p_{1s} = 0.5 \text{ bar} , h_{1s} = 1.4 \text{ m} , v_{1s} = 0.4152 , v_{2s} = 0.7462$$

$$\mathbf{x}(t+1) = \mathbf{A}\mathbf{x}(t) + \mathbf{B}u(t)$$

$$\mathbf{A} = \begin{bmatrix} 0.9719 & -0.0001 \\ -0.0006 & 0.9999 \end{bmatrix}, \quad \mathbf{B} = \begin{bmatrix} -0.0832 & -0.0041 \\ 0 & -0.0023 \end{bmatrix}$$

$$\mathbf{x}_1 = p_1 - p_{1s} [\text{bar}] , \quad \mathbf{x}_2 = h_1 - h_{1s} [\text{m}]$$

$$\mathbf{u}_1 = v_1 - v_{1s} , \quad \mathbf{u}_2 = v_2 - v_{2s}$$

Two more states are added to take into account the integral error:

$$\mathbf{x}_3(t+1) = \mathbf{x}_3(t) + T_s \mathbf{x}_1(t)$$

$$\mathbf{x}_4(t+1) = \mathbf{x}_4(t) + T_s \mathbf{x}_2(t)$$

$$\mathbf{A} = \begin{bmatrix} 0.9719 & -0.0001 & 0 & 0 \\ -0.0006 & 0.9999 & 0 & 0 \\ T_s & 0 & 1 & 0 \\ 0 & T_s & 0 & 1 \end{bmatrix}, \quad \mathbf{B} = \begin{bmatrix} -0.0832 & -0.0041 \\ 0 & -0.0023 \\ 0 & 0 \\ 0 & 0 \end{bmatrix}$$

## Constraints:

$$0 \leq v_1 \leq 1$$

$$0 \leq v_2 \leq 0.8625$$

$$-0.33 \leq \dot{v}_1 \leq 0.66$$

$$-0.33 \leq \dot{v}_2 \leq 0.66$$

Constraints on control variables:

$$-0.4152 \leq \mathbf{u}_1(\mathbf{t} + \mathbf{k}) \leq 0.5848 \quad , \mathbf{k} = 0, 1, \dots, \mathbf{N} - 1$$

$$-0.7462 \leq \mathbf{u}_2(\mathbf{t} + \mathbf{k}) \leq 0.1163 \quad , \mathbf{k} = 0, 1, \dots, \mathbf{N} - 1$$

Constraints on the rate of change of control variables:

$$-0.33T_s \leq \mathbf{u}_1(\mathbf{t} + \mathbf{k}) - \mathbf{u}_1(\mathbf{t} + \mathbf{k} - 1) \leq 0.66T_s \quad , \mathbf{k} = 1, 2, \dots, \mathbf{N} - 1$$

$$-0.33T_s \leq \mathbf{u}_2(\mathbf{t} + \mathbf{k}) - \mathbf{u}_2(\mathbf{t} + \mathbf{k} - 1) \leq 0.66T_s \quad , \mathbf{k} = 1, 2, \dots, \mathbf{N} - 1$$

Horizon:  $N=500$

Control input parameterization:

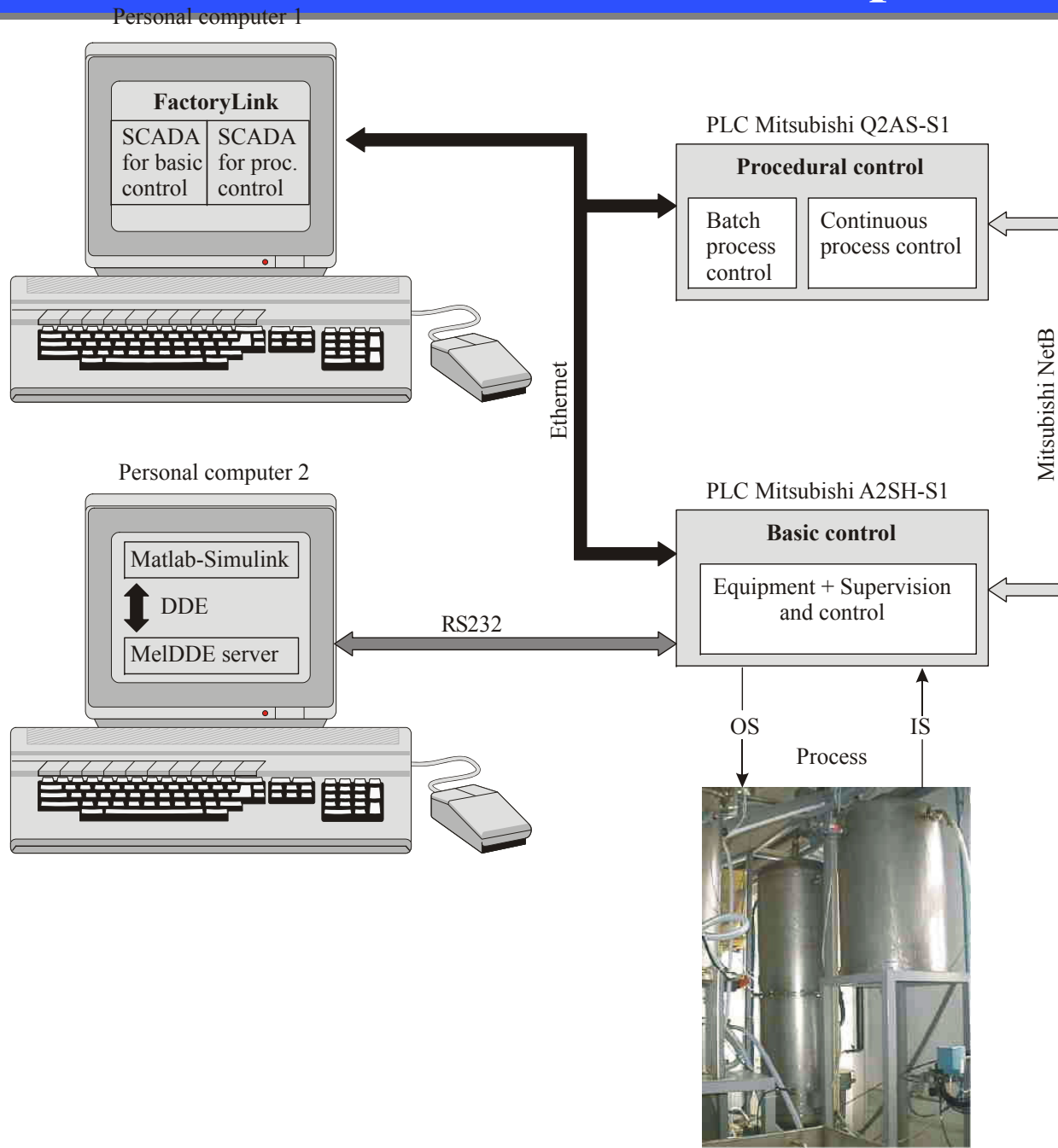
$$N_{u_1} = [1 \ 5 \ 10 \ 15 \ 20 \ 25 \ 30 \ 35 \ 40 \ 45 \ 50 \ 100 \ 102 \\ 104 \ 106 \ 108 \ 110 \ 300 \ 302 \ 304 \ 306 \ 308 \ 310]$$

$$N_{u_2} = [1 \ 5 \ 10 \ 15 \ 20 \ 25 \ 30 \ 35 \ 40 \ 45 \ 50 \ 100 \ 300]$$

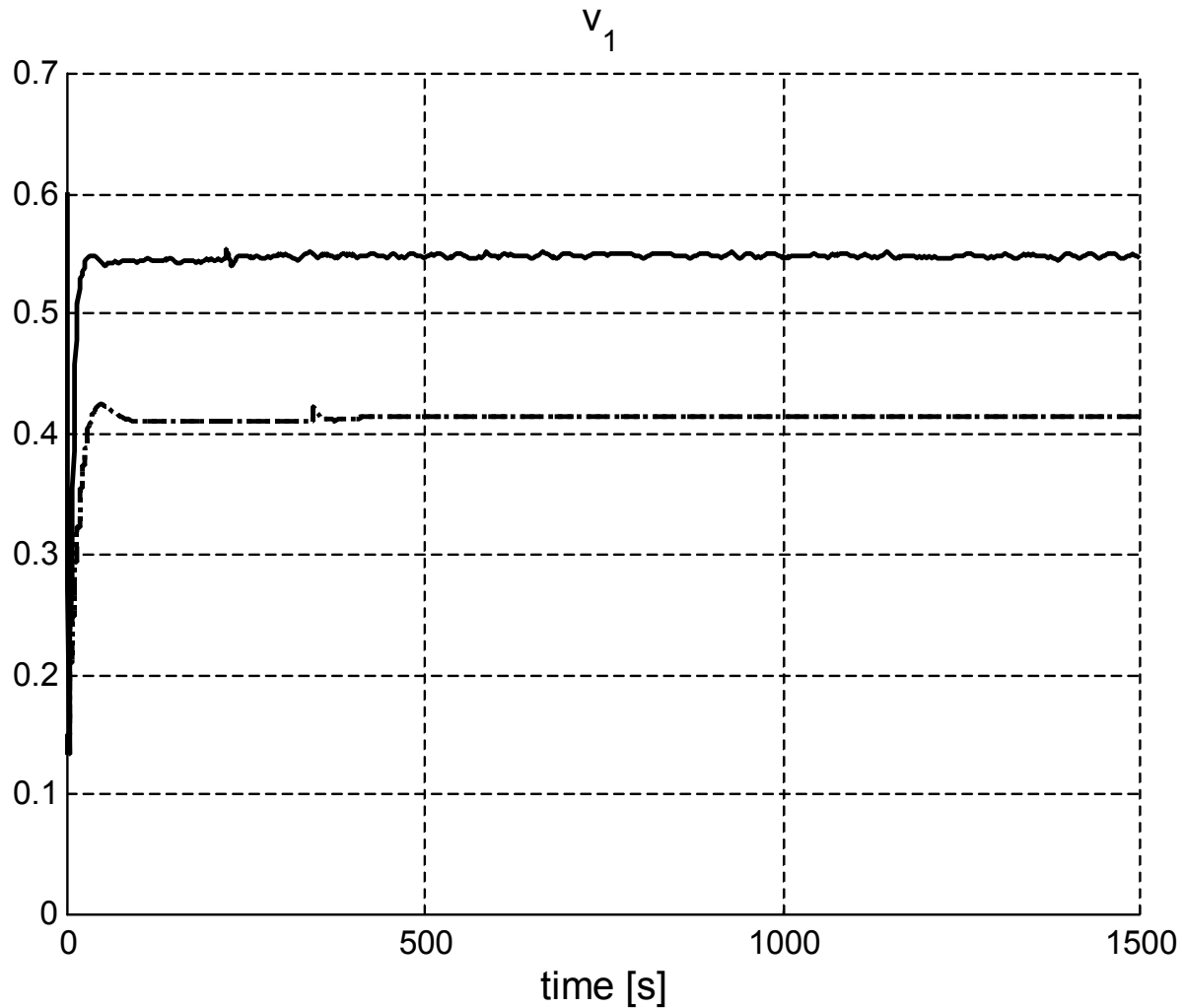
Cost matrices:

$$Q = \text{diag}\{0.05, 100, 0.005, 0.0001\}, R = \text{diag}\{1, 1\}$$

# Environment for the real-time experiments

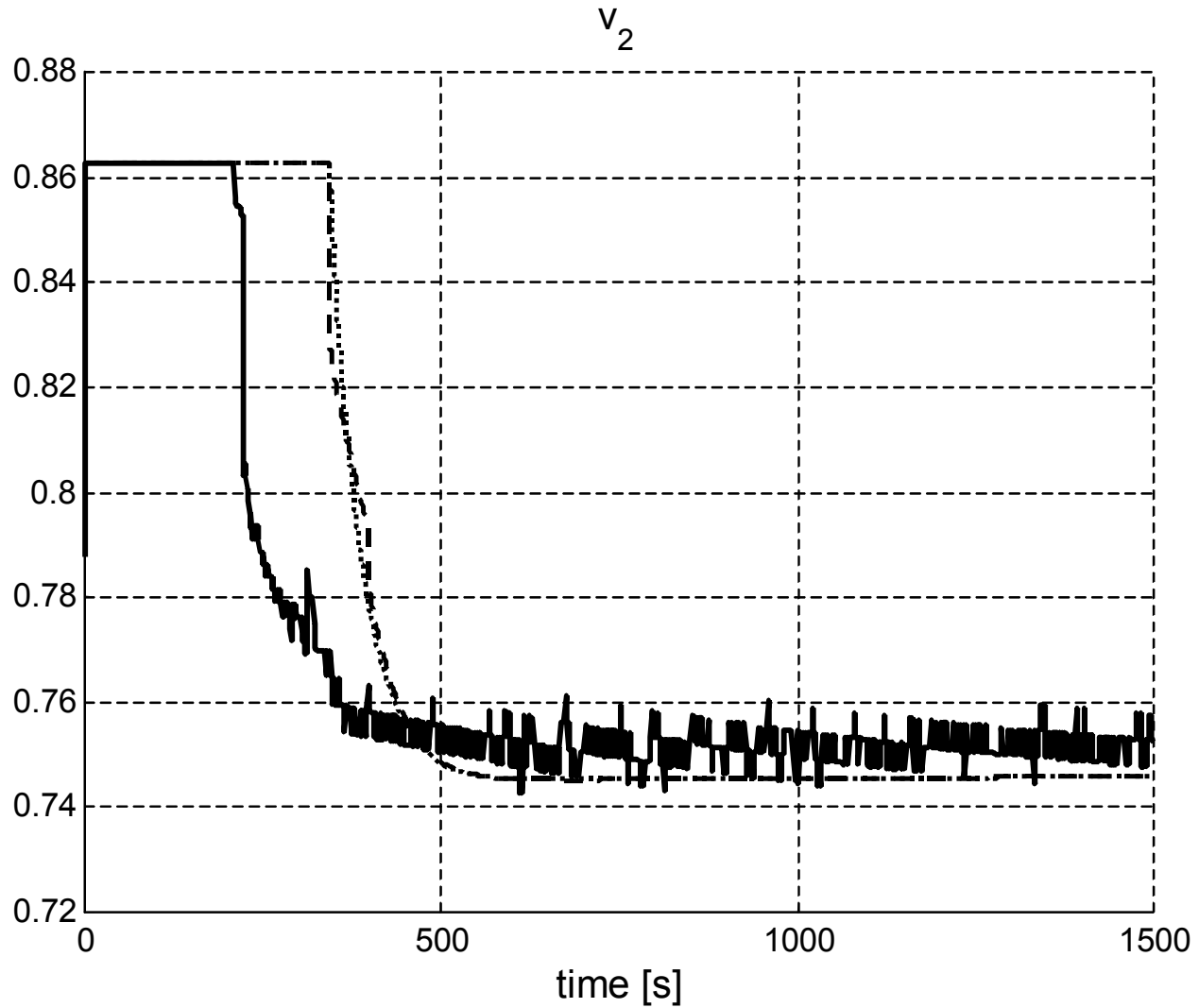


# Real-time performance of the MPC controller

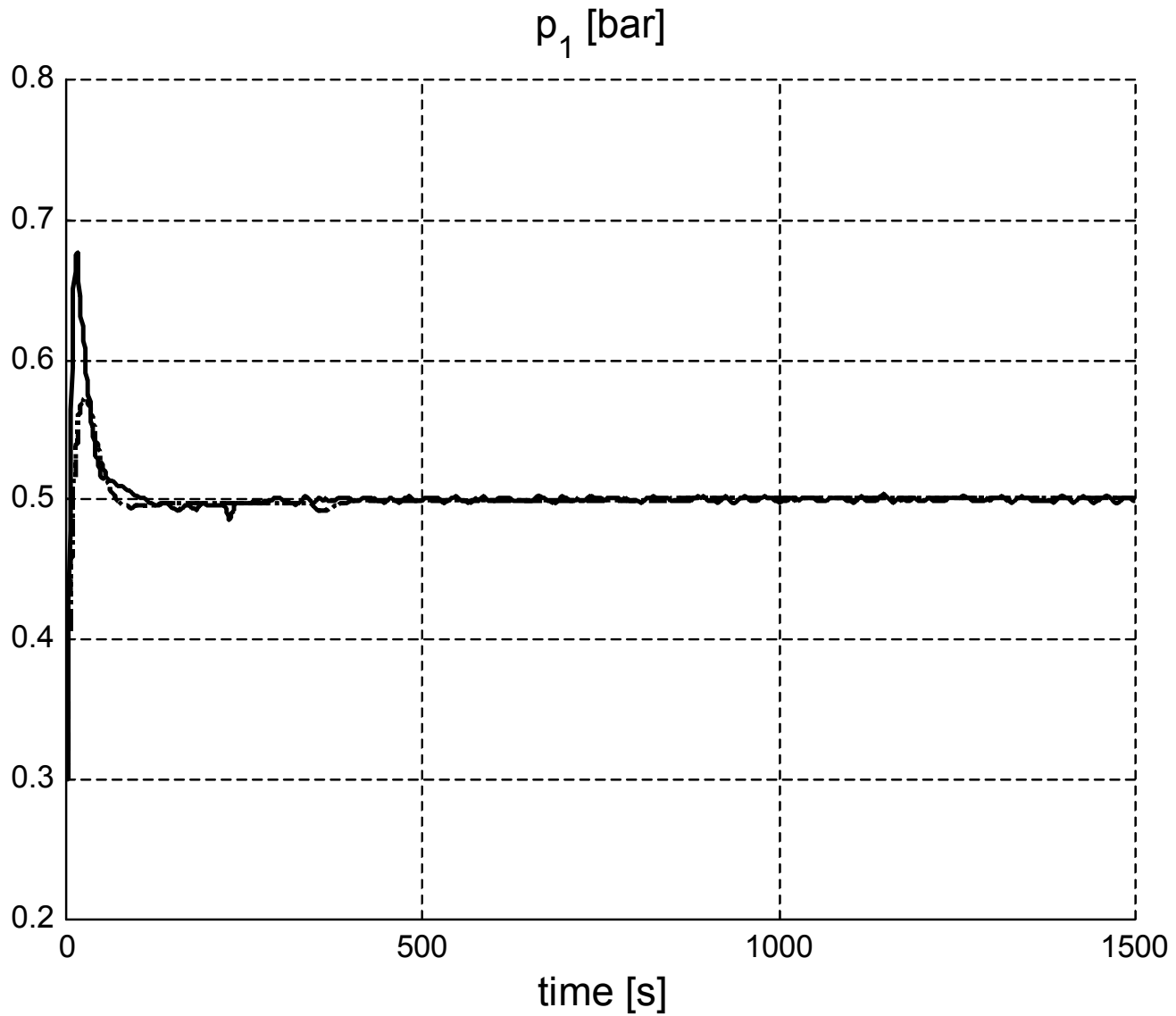


Valve 1  
— experiments  
... exact  
-- simulated

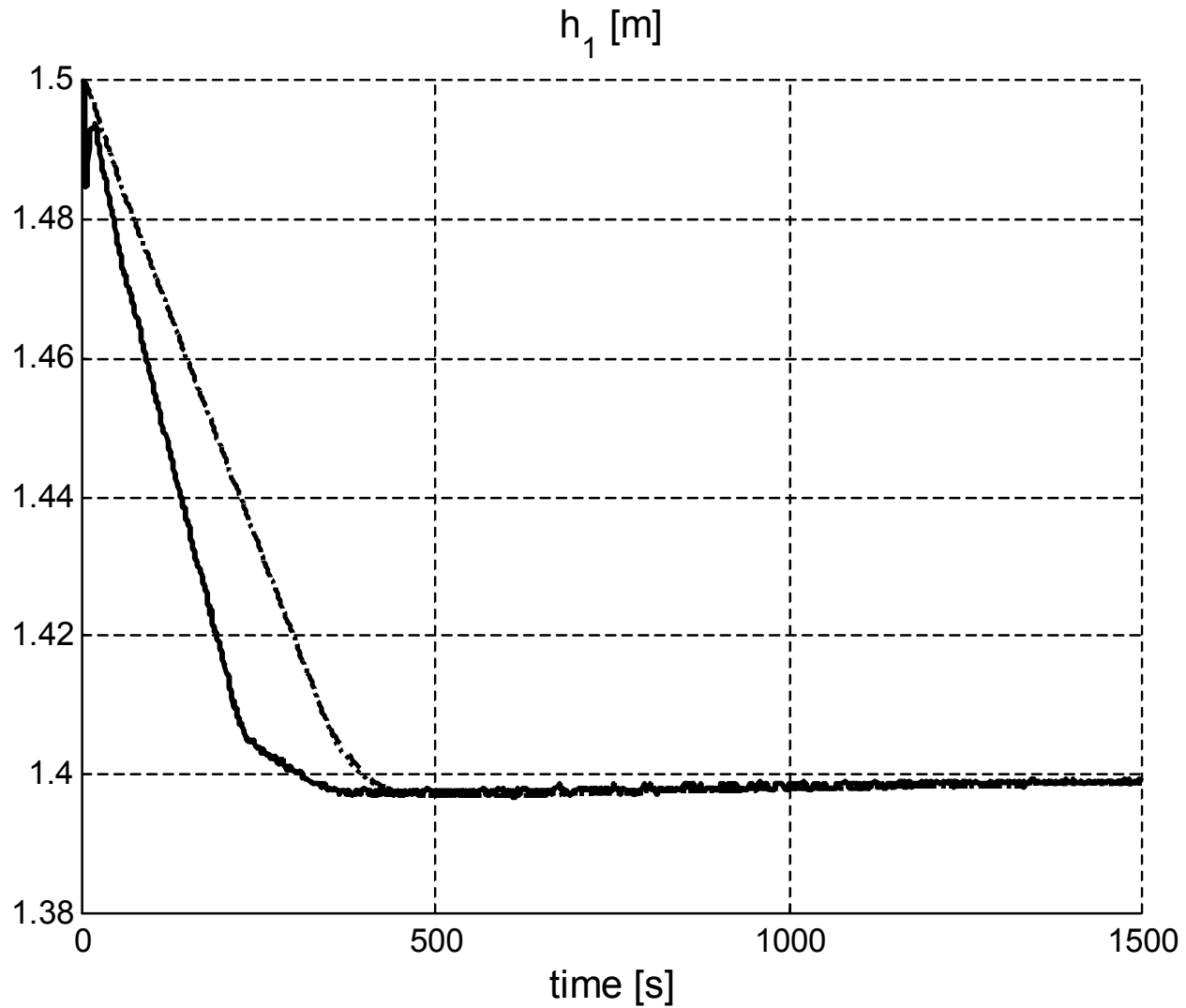




Valve 2 (— experiments, ... exact, - - - simulated)

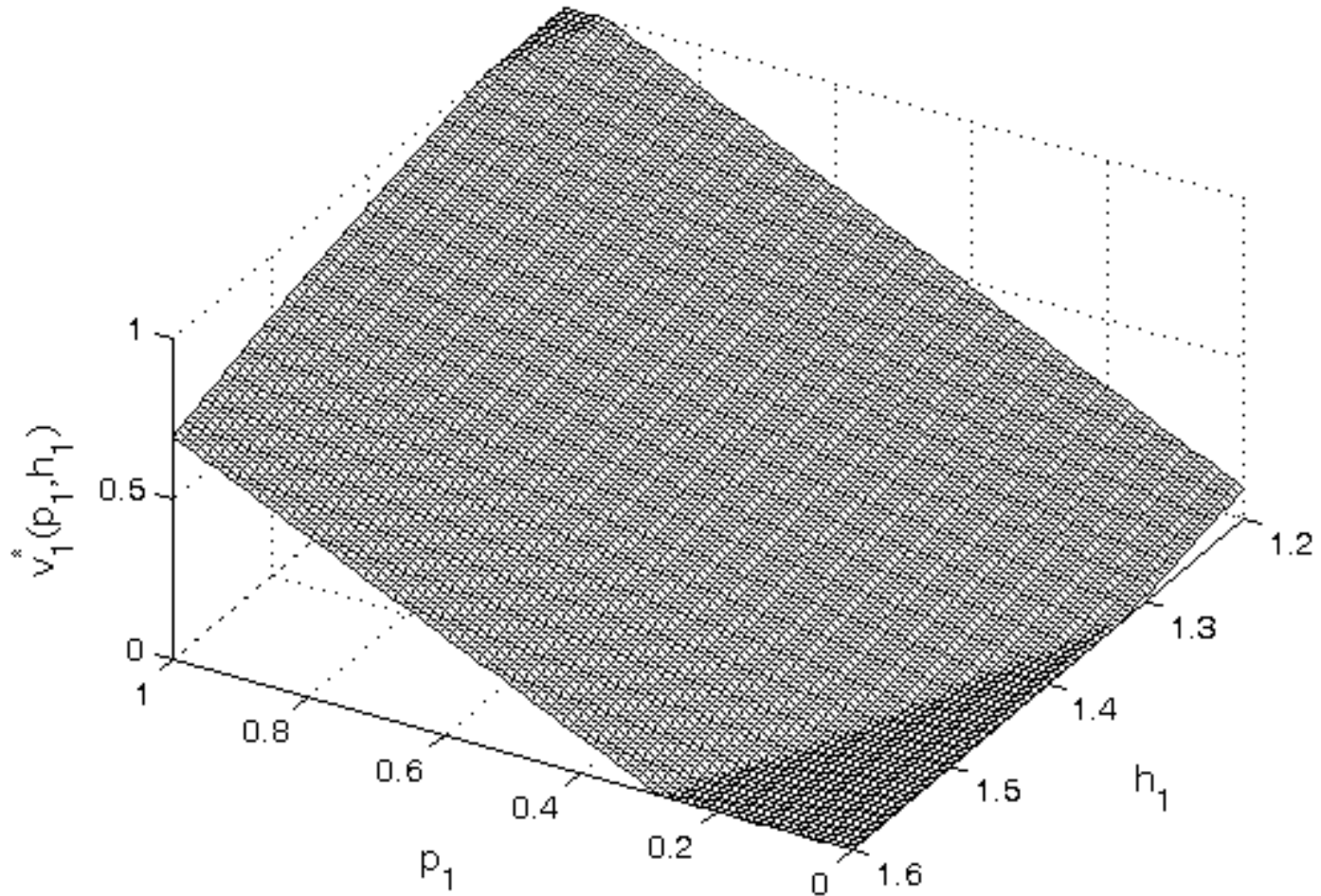


Pressure (— experiments, ... exact, - - - simulated)



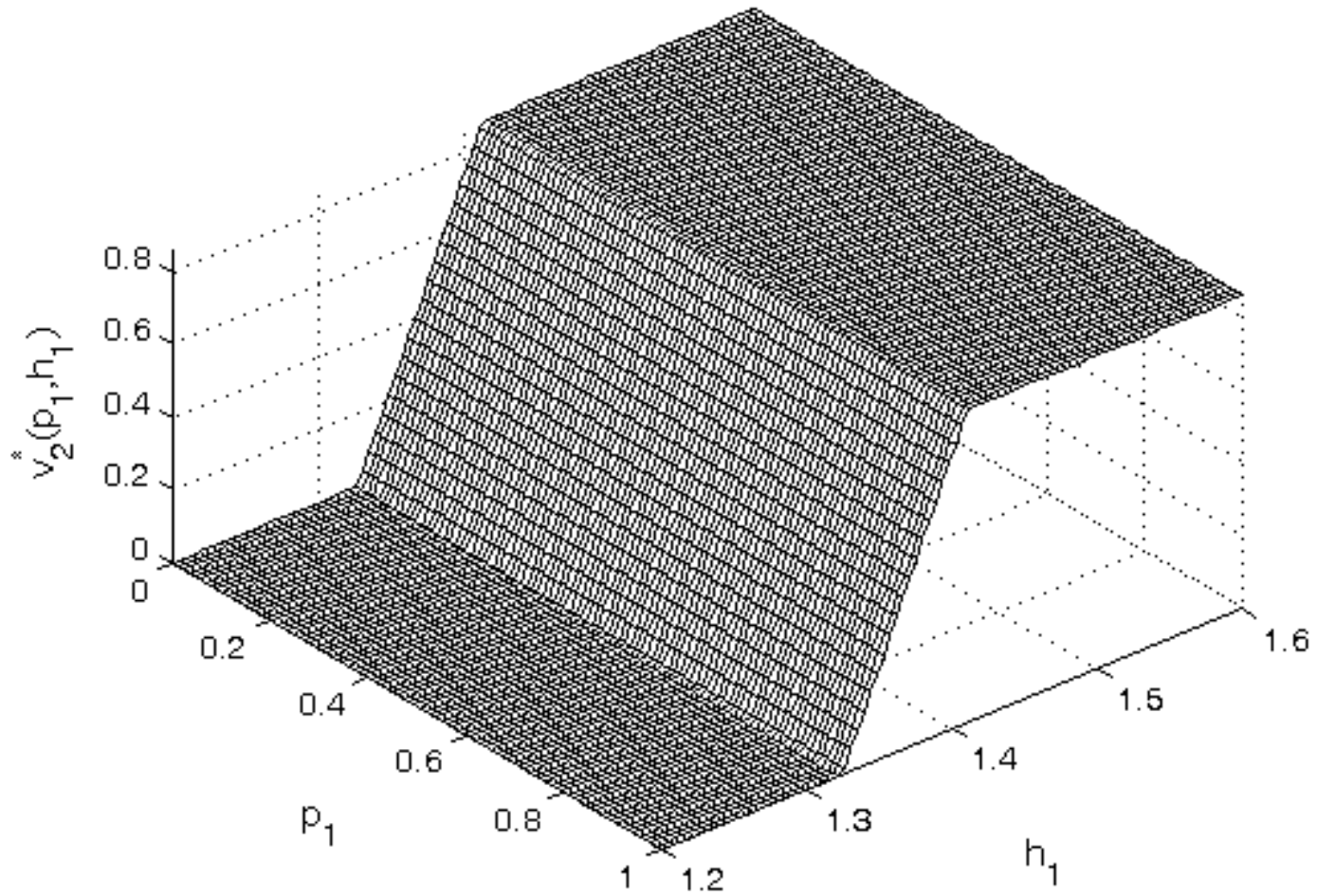
Liquid level (— experiments, ... exact, - - - simulated)

# Valve 1



Feedback law  $v_1(p_1, h_1)$

# Valve 2



Feedback law  $v_2(p_1, h_1)$

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